AMENDMENTS TO THE CLAIMS

1. (currently amended) A method for controlling the flowability of polymer particles ~~flowing downward in a densified form inside a polymerization reactor, in which one or more monomers are gas phase polymerized in the presence of a polymerization catalyst, the density of solid (Kg of polymer per m^3 of reactor occupied by the polymer) being higher than 80% of the "poured bulk density" of the polymer, the method being characterized in that a liquid stream is continuously fed into the polymerization reactor at a mass flow rate per unity of reactor surface higher than 30 Kg/h m^2~~comprising:

   feeding a liquid stream continuously into a polymerization reactor comprising a polymer bed at a mass flow rate per unity of reactor surface higher than 30 Kg/h-m^2,

   wherein the polymer particles comprise a polymer and a density of solid higher than 80% of a poured bulk density of the polymer, where the density of solid is the Kg of polymer per m^3 of reactor occupied by the polymer, and the polymer particles flow downward in a densified form inside the polymerization reactor, wherein at least one monomer is gas phase polymerized in the presence of a polymerization catalyst, the monomer comprising fresh monomers.

2. (currently amended) The method according to claim 1, wherein said liquid stream is fed at a mass flow rate per unity of reactor surface in the range from 50 to 200 Kg/h m^2.

3. (currently amended) The method according to ~~any of claims 1-2~~claim 1, wherein said liquid stream is obtained from the condensation of a part of the fresh monomers ~~to be polymerized~~.

4. (currently amended) The method according to ~~any of claims 1-2~~claim 1, wherein said liquid stream ~~comes from the~~is obtained from cooling and condensation of ~~the~~a recycle gas stream.

5. (currently amended) The method according to claim 4, wherein said liquid stream ~~contains, besides~~comprises the at least one monomer and ~~the monomers to be polymerised, also~~ condensable inert compounds[[,]] selected from aliphatic hydrocarbons C_2-C_8.

6. (currently amended) The method according to ~~any of claims 1-5~~claim 1, wherein the feeding of said liquid stream is equally distributed along the reactor by ~~means of more~~at least one feeding ~~lines~~line, the number of said feeding lines being an integer ~~equal or higher than~~at least equal to 0.2xH, where H is the height ~~(expressed~~ in meters~~)~~ of the polymer bed ~~inside the reactor~~.

7. (currently amended) The method according to claim 1, wherein said ~~one or more monomers are α-olefins~~at least one monomer is an α-olefin of formula CH_2=CHR, where R is hydrogen or a hydrocarbon radical having 1-12 carbon atoms.
8. (currently amended) The method according to ~~any of claims 1-7~~claim 7, wherein said α-olefins are gas-phase polymerized in a first polymerization zone and ~~in~~ a second polymerization zone comprising a polymer bed, the first and second polymerization zones being interconnected~~inter-connected polymerization zones~~, where the ~~growing~~ polymer particles flow through the first ~~of said~~ polymerization ~~zones~~zone under fast fluidization conditions, leave said first polymerization zone and enter the second ~~of said~~ polymerization ~~zones~~zone through which they flow downward in a densified form, leave said second polymerization zone and are reintroduced into said first polymerization zone, thus establishing a circulation of polymer between said two polymerization zones.
9. (currently amended) The method according to ~~any of claims 1-8~~claim 8, wherein said liquid stream is continuously fed into said second polymerization zone.
10. (currently amended) The method according to ~~any of claims 8-9~~claim 9, wherein the feeding of said liquid stream is equally distributed along the height of said second polymerization zone by ~~means of more feeding lines~~at least one feeding line, the number of said feeding lines being an integer ~~equal or higher than~~at least equal to 0.2xH, where H is the height ~~(expressed~~ in meters~~)~~ of the second polymerization zone polymer bed ~~inside said second polymerization zone~~.